APPENDIX I:

CLAIM AMENDMENTS:

Cancel Claims 13 and 18 to 20, amend Claims 12 and 27, and enter new Claims 28 to 35, as indicated in the following listing of the claims:

1. - 11. (canceled)

- 12. (currently amended) A process for preparing highly reactive polyisobutenes having a terminal vinylidene group content of more than 80 mol% and an a number average molecular weight of from 500 to 5000 dalton by cationic polymerization of isobutene in the liquid phase in the presence of a complex comprising boron trifluoride at from +40° to -60°C, which comprises polymerizing isobutene in the presence of a complex comprising boron trifluoride and
 - a) a primary alcohol having 1-20 carbon atoms or a secondary alcohol having 3-20 carbon atoms, or a mixture of these alcohols, and
 - b) an ether containing no tertiary alkyl groups and having the formula I

R1-O-R2 I.

wherein R^1 is a secondary alkyl group having 3-10 carbon atoms, and R^2 is methyl, ethyl, or a primary or secondary alkyl group having 3-10 carbon atoms,

wherein the alcohol (a) and the ether (b) have a molar ratio of from 0.01:1 to 1:1, and the molar ratio of the sum of alcohol (a) and ether (b) to boron trifluoride is more than 1 and less than 2

wherein the molar ratio of the sum of alcohol (a) and ether (b) to boron trifluoride is from 1.4:1 to 2:1.

13. (canceled)

- 14. (previously presented) A process as claimed in claim 12, wherein the molar ratio of the alcohol (a) to the ether (b) is from 0.2:1 to 1:1.
- 15. (previously presented) A process as claimed in claim 12, wherein the molar ratio of the alcohol (a) to the ether (b) is from 0.4:1 to 1:1.

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- 16. (previously presented) A process as claimed in claim 15, wherein the alcohol (a) is isopropyl alcohol and/or 2-butanol.
- 17. (previously presented) A process as claimed in claim 15, wherein the ether (b) is diisopropyl ether, di-sec-butyl ether and/or isopropyl sec-butyl ether.
- 18. 20. (canceled)
- 21. (previously presented) A process as claimed in claim 12, wherein the alcohol (a) is isopropyl alcohol and/or 2-butanol.
- 22. (previously presented) A process as claimed in claim 12, wherein the ether (b) is diisopropyl ether, di-sec-butyl ether and/or isopropyl sec-butyl ether.
- 23. (previously presented) A process as claimed in claim 12, wherein boron trifluoride, the alcohol (a) and the ether (b) are combined in the polymerization reactor to generate the complex in situ in the polymerization mixture.
- 24. (previously presented) A process as claimed in claim 12, wherein a complex of boron trifluoride and the ether (b) is preformulated and is introduced into the solvent or monomer feed to the reactor or directly into the reactor, either separately or together with the alcohol (a).
- 25. (previously presented) A process as claimed in claim 12, wherein polyisobutenes having a terminal vinylidene group content of more than 90 mol% are polymerized at an isobutene conversion of up to 95% using a preformed complex of boron trifluoride/isopropanol/diisopropyl ether, having a molar ratio of isopropanol to diisopropyl ether of from 2:1 to 1:5 and a molar ratio of boron trifluoride to diisopropyl ether of from 0.6:1 to 0.9:1.
- 26. (previously presented) A process as claimed in claim 12, wherein the isobutene source is a C_4 cut comprising isobutene in an amount of at least 6% by weight.
- 27. (currently amaended) A polyisobutene having an a number average molecular weight of from 500 to 5000 dalton and a terminal viny-lidene group content of more than 90%, obtainable obtained by cationic polymerization of isobutene in the liquid phase with the aid of boron trifluoride as catalyst at from 40 to -60°C in the presence of a boron trifluoride complex with

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- a) a primary alcohol having 1-20 carbon atoms or a secondary alcohol having 3-20 carbon atoms, or a mixture of these alcohols, and
- b) an ether containing no tertiary alkyl groups and having the formula I

R1-O-R2

wherein R1 is a secondary alkyl group having 3-10 carbon atoms, and R2 is methyl, ethyl, or a primary or secondary alkyl group having 3-10 carbon atoms,

wherein the alcohol (a) and the ether (b) have a molar ratio of from 0.01:1 to 1:1, and the molar ratio of the sum of alcohol (a) and ether (b) to boron trifluoride is more than 1 and less than 2

wherein the molar ratio of the sum of alcohol (a) and ether (b) to boron trifluoride is from 1.4:1 to 2:1.

- 28. (new) A polyisobutene as claimed in claim 27, wherein the molar ratio of the alcohol (a) to the ether (b) is from 0.2:1 to 1:1.
- 29. (new) A polyisobutene as claimed in claim 27, wherein the molar ratio of the alcohol (a) to the ether (b) is from 0.4:1 to 1:1.
- 30. (new) A polyisobutene as claimed in claim 29, wherein the alcohol (a) is isopropyl alcohol and/or 2-butanol.
- 31. (new) A polyisobutene as claimed in claim 29, wherein the ether (b) is diisopropyl ether, di-sec-butyl ether and/or isopropyl sec-butyl ether.
- 32. (new) A polyisobutene as claimed in claim 27, wherein the alcohol (a) is isopropyl alcohol and/or 2-butanol.
- 33. (new) A polyisobutene as claimed in claim 27, wherein the ether (b) is diisopropyl ether, di-sec-butyl ether and/or isopropyl sec-butyl ether.
- 34. (new) A process as claimed in claim 12, wherein the terminal vinylidene group content is of more than 90%.
- 35. (new) A process as claimed in claim 15, wherein the terminal vinylidene group content is of more than 90%.

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